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Use of metallics in electric arc furnace steelmaking

Presentation at the American Metal Markets conference on DRI and Mini mills in Chicago 2016-11-16--18

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Abstract: In this study, steelmaking in an Electric Arc Furnace, EAF, using two types of recycled scrap with different levels of tramp-Cu and different prices, is compared to steelmaking where part of the burden is changed to a virgin iron source. By using the tool RAWMATMIX® for optimizing EAF charges, a Value in Use, ViU, is calculated for Pig Iron, three different types of DRI with different temperature and MgO content and a commercial HBI with high Silicon. The result shows that the ViU per ton material differs from +3 % to -20 % for different sources. Using virgin material also affects the environmental profile of the product and especially the Global Warming Potential, with different CO₂ burdens depending on source. The paper shows the importance of making ViU calculations when establishing a raw material price.

Key words: Electric arc furnace, Scrap, DRI, HBI, Pig Iron, Tramp element, Global Warming Potential, Value in use

1. Background

Steel is a 100% recyclable material. Obsolete products together with new scrap coming from production, are collected, sorted and formatted to fit into different classes according to some classification system. Each class states the allowed geometry, density, thickness, levels of alloying elements or pickable metal parts, coatings, steriles, sources for the material etc. One example of a system for specifying the different classes is the Scrap Specifications Circular [1].

Tramp elements are unwanted alloys that occur in scrap. They may have many different origins, but usually some main sources can be identified. Copper is used in bearings and electrical wire and is often found in scrap. In scrap that comes from recycled steel the copper content in the steel matrix is often higher than in scrap that comes from blast furnace steel. Most steels are sensitive to the cupper content. Thus, in many plants it is the only element considered in charge optimization. Other examples of elements that occurs as tramp elements are Nickel and Chromium coming from ferritic alloyed steel scrap; and tin and lead which often come from different kinds of coatings and bearings [2].

For a steelmaker it is important to know the analysis and uncertainty of the scrap in order to avoid getting to much of a tramp element into the steel. A steel charge normally consists of about ten different scrap types, which are blended to give the right analysis and smelting properties at the lowest possible cost. When the demands on low levels of tramp elements are high, scrap sources with a known analysis must be used. This can be new scrap from known sources or virgin material from ore like Blast Furnace Iron or Direct Reduced Iron.

By using Life Cycle Analysis, LCA, the environmental

load from primary production of steel from ore and secondary production of steel from scrap can be scrutinized. Although it is right to argue that there can be no scrap based steelmaking unless there has been a primary steelmaking first, it is important to understand how different sources changes the load. The way to report the impacts are given in a number of standards and for the Global Warming Potential an ISO technical specification also exist [3]. Using virgin material together with recycled material adds a twist to this question, which is discussed later in the paper.

2. Method

In this study, we have chosen to set a market price to scrap of a premium and second quality and then estimate the Value in Use, ViU, for the virgin iron sources. No 1 heavy melting steel is a heavy old scrap, in this case with a Cu limit of 0.25% and X is a similar scrap with a Cu limit of 0.4%. Prices are averages representative for a period with intermediate levels, basically from 2014[4]. The calculation base is 100 tons of steel with a Cu-limit of 0.22%. In the reference charge we use 100 % scrap and in the virgin charges we use 60 ton scrap and the rest virgin material.

The steel is produced in a modern EAF with burners using Liquid Petrol Gas, LPG. We strive for a slag that contains 20% FeO, 38% CaO as well as a 10% MgO oversaturation to reduce refractory wear. The same amount of time for charging the different raw materials to the furnace is assumed. The virgin materials are: pig iron, PI, which is a commodity that is traded globally, two types of DRI from a natural gas based shaft furnace and finally a commercial HBI which again is a globally traded commodity. The pig iron has the analysis of a normal blast furnace iron which is low in Si. The first DRI is a low-Si and high MgO containing DRI typical for the Gulf area and the USA. The second DRI has a slightly lower MgO content. Finally, the HBI is a standard commercial grade with a higher Si content. It is worth noting that the chemical composition of DRI and HBI is totally dependent on the composition of the ore. The software RAWMATMIX® calculates the raw material mix that meets the product requirements at lowest possible cost. It uses the MgO saturation model presented by Selin [5] to calculate lowest possible amount of slag former addition to meet the slag requirements. Dust is calculated as a percentage of metals melted and a percentage of the fine fraction of the raw materials. This comparison is simplified in the way that it is assumed that no difference between carbon in the raw material and inject carbon exists. The yield for injected carbon is however often lower than for carbon in the metallics.

When estimating the ViU for a material x the difference between the production cost for a reference case, C_{ref} , and the production cost for a case using material x, C'_x , is divided by the amount of material x, w_x . C'_x does not include the cost for x and the result will be the price for x that would result in the same production cost as the reference case everything else alike. It could be expressed as in equation 1.

$$ViU_x = \frac{C_{ref} - C_x'}{w_x}$$

The ViU may be higher or lower than the market price. Thus if it is higher you should buy and if it is lower you should avoid buying. It is evident that the ViU is strongly dependent on the reference case which should be representative for the normal practice you use for the steel product for which you consider to use the alternative material. Furthermore, the calculations are simplified and do not reflect real burdens in all aspects. However, the method gives an opportunity to investigate the intrinsics of different materials and how they are priced.

3. Calculation data

A number of production parameters used in the calculations are shown in Table 1.

| Tuble 1 1 Toutetion parameters | | | | | | |
|--------------------------------|--------|-------------------------|--|--|--|--|
| Parameter | Amount | Unit | | | | |
| Furnace burners | 5000 | kWh/charge | | | | |
| Oxygen for slag foaming | 3000 | Nm ³ /charge | | | | |
| Electrode consumption | 4.38 | kg/MWh | | | | |
| Process water | 10 | m ³ /min | | | | |
| Tapping temperature | 1600 | °C | | | | |
| Tap weight | 100 | ton | | | | |
| Average power on | 45 | MW | | | | |
| Average power off /idle time | 5/4 | min | | | | |
| Power on/idle heat loss | 5 /4 | MW | | | | |
| Idle/Power off heat loss | 1 | MW | | | | |
| Post combustion | 6 | % in furnace | | | | |
| Dust from lime in EAF | 1 | % | | | | |
| Dust generated in arc | 1 | % | | | | |

Table 1 Production parameters*

* Parameter data are examples collected from industrial furnaces

The data used for raw materials are shown in Table 2. Important figures to note are the Cu-content and the Fe_{tot} value. Other raw material data are shown in Table 3 and other cost data in Table 4.

Table 2 Raw material properties

| | Indica | | muttim | i properu | 0.5 | |
|---|--------|-------|--------|--------------------|-------|-------|
| | NO 1 | Х | PI | DRI1 | DRI2 | HBI |
| Fe | 95 | 94.3 | 94 | 84.57 | 84.57 | 82.74 |
| С | 0.4 | 0.4 | 4.2 | 2 | 2 | 2 |
| Si | 0.3 | 0.3 | 0.5 | | | |
| Mn | 0.8 | 0.8 | 0.2 | | | |
| Cu | 0,2 | 0.4 | 0 | | | |
| FeO | 2 | 2 | 1 | 9.46 | 9.46 | 9.24 |
| CaO | | | | 1.1 | 1.1 | 0.93 |
| MgO | | | | 0.35 | 0.35 | 0.23 |
| SiO ₂ | 0.5 | 1 | | 1.48 | 1.48 | 4.55 |
| Al ₂ O ₃ | 0.5 | 0.5 | | 0.56 | 0.56 | 0.24 |
| Other | 0.5 | 0.3 | 0.1 | 0.48 | 0.48 | 0.07 |
| Fet _{ot} | 96,56 | 95,86 | 94,78 | 91,95 | 91,95 | 89,95 |
| Met | | | | 92% | 92% | 92% |
| Temp C | 25 | 25 | 25 | Hot 500 Cold 25 | 25 | 25 |
| Price (USD) [4] | 264 | 240 | - | - | - | - |
| Upstream CO ₂ (kg CO ₂ eq) [6] | 0 | 0 | 1.35 | 0.7 | 0.7 | 0.7 |

Table 3 Other raw material and energy data

| Raw material | Price * | Upstream CO ₂ | Comments | | | |
|---|---|--------------------------|--------------------|--|--|--|
| | (USD) | ** (kg CO2eq) | | | | |
| Burnt Lime (kg) | 0.12 | 1.24 [7] | 100% CaO | | | |
| Burnt Dolomite (kg) | 0.15 | 1.63 [7] | 30% MgO | | | |
| | | | 70% CaO | | | |
| Magnesite bricks (kg) | 1 | 4.01 [7] | 100% MgO | | | |
| Inject coal (kg) | 1 | 0,012 | 53 kWh/ton [8] | | | |
| Electrodes (kg) | 4 | 1,58 | 24,5 GJ/ton [9] | | | |
| LPG (GJ) | 20 | 8 [10] | 55 Nm3 O2/GJ | | | |
| Electricity (kWh) | 0.15 | 1.0 | Average fossil el. | | | |
| Oxygen (Nm ³) | 0,1 | 0.661 | Average fossil el. | | | |
| Process water (m ³) | 0,1 | 0.344 | | | | |
| CO2 emission used for process and estimation of upstream emission | | | | | | |
| Natural Gas (GJ) | al Gas (GJ) 64.6 kg CO ₂ /GJ | | | | | |
| LPG (GJ) | 65.7 kg CO ₂ /GJ | | | | | |
| Inject Carbon | 3.7 kg CO ₂ /kg | | | | | |
| Electrodes | 3.7 kg CO ₂ /kg | | | | | |
| * Prices are average prices from 2014-2016 [2] | | | | | | |

* Prices are average prices from 2014-2016 [2].

** Due to shortage information, upstream CO₂ for burnt lime, dolomite, magnesite bricks, inject coal does not include CO2 emission from mining process and transportation between mining and production plant.

Table 4 Other costs

| Tuble 1 Other costs | | | | | | |
|---------------------|--------------|--|--|--|--|--|
| Amount | Unit | | | | | |
| 20 | USD | | | | | |
| 40 | USD | | | | | |
| | Amount 20 | | | | | |

Calculation result

The optimized burden is shown in Table 5. The reference calculation, "Scrap", uses almost only the more expensive NO 1 as burden. The virgin materials that all lack Cu can use the less expensive X. The slag formers show that the HBI charge needs more dolomite than the others to balance the high Si content. In this evaluation, the charge time is left out.

| Charge | Scrap | PI | HDRI | DRI1 | DRI2 | HBI | | | |
|----------------------------|--------|--------|--------|--------|--------|--------|--|--|--|
| NO 1 | 99,337 | 21,280 | 24,278 | 24,278 | 24,349 | 27,105 | | | |
| X | 5,890 | 44,918 | 43,419 | 43,419 | 43,384 | 42,006 | | | |
| Fe-alt | 0 | 40,000 | 40,000 | 40,000 | 40,000 | 40,000 | | | |
| Lime | 1,636 | 1,307 | 1,351 | 1,351 | 1,231 | 1,625 | | | |
| Dolo | 2,012 | 2,067 | 2,294 | 2,294 | 2,579 | 3,851 | | | |
| Coal | 2,131 | 559 | 2,126 | 2,126 | 2,118 | 1,971 | | | |
| | | | | | | | | | |
| Total energy kWh | 56380 | 54125 | 55746 | 58533 | 59258 | 67264 | | | |
| Slag volume tons | 7,985 | 7,231 | 8,941 | 8,941 | 9,149 | 12,348 | | | |
| Direct cost* USD/ton | 348,97 | 223,22 | 236,35 | 241,65 | 242,44 | 256,92 | | | |
| ViU** USD/ton | 264,00 | 314,38 | 281,55 | 268,30 | 266,32 | 230,12 | | | |
| +/- | | 50,38 | 17,55 | 4,30 | 2,32 | -33,89 | | | |
| % | | 19,08 | 6,65 | 1,63 | 0,88 | -12,84 | | | |

Table 5 Charged materials, energy, slag volume and costs

*The price for metallics is set to 0

** The price for scrap or metallics giving the same direct cost.

Finally, it should be noted that when using virgin materials, the environmental profile of a material changes. According to the standards for LCA and environmental declarations [3], a recycled material comes free of upstream environmental burden for the period before it reached the "end of waste" status. A virgin material must carry its environmental burden, but can declare a credit that it can be recycled and replace steel from virgin materials. However, it is important to understand the carbon metrics in order to appreciate the environmental declarations and to communicate the environmental performance.

Table 9 Global Warming Potential expressed as kg CO₂/ton.

| | Scrap | PI | HDRI | DRI1 | DRI2 | HBI |
|-----------------------------|-------|------|------|------|------|-----|
| CO ₂ Process | 114 | 112 | 138 | 138 | 137 | 133 |
| CO ₂ Upstream | 301 | 964 | 608 | 640 | 646 | 715 |
| CO2 Total | 415 | 1076 | 746 | 777 | 783 | 848 |

* Upstream CO2 for Fe-materials left out

Upstream CO₂ is the main emission that is caused when producing the raw materials and energy products. Process CO₂ is the emissions from the process itself. Most of the upstream CO₂ from scrap comes from electricity and the virgin materials from the reduction process. In this example a coal- based electricity is used. However, the figure for scrap would change drastically if for example nuclear power was used instead.

4. Discussion

To draw conclusions from cost calculations is always tricky, since raw material prices are highly volatile. With the ViU calculation using scrap as a reference case you can avoid some of the uncertainties of comparing assumed actual costs. In these calculations, we take chemical properties and thermodynamics into account whereas other aspects must be left out and dealt with in a more case based reasoning way.

The approach used here is favourable to metallics since we have assumed the same furnace parameters for all burdens. A slower melting down, possibility to avoid a second basket together with injection capacity make a great difference. Furthermore, the price relation between good and bad scrap, electricity and coal set the scene.

Different types of virgin materials might require some adjustments to the burdening and the process equipment, like charging through the roof of the furnace. Issues that are often discussed are the amount of metallics that can be charged in the furnace and 20-40 % is mentioned when it is charged together with scrap in the first bucket, less for HBI than for DRI and even less for PI. A big advantage is the higher density of metallics that makes the charging more efficient. [12]. The higher carbon content improves the CO_2 generation within the melt, which result in lower nitrogen levels [13] and decreases the need for carbon injection but may make HBI and Pig Iron harder to melt [12].

Using virgin material in order to abate the level of tramp elements will probably be a more common practice in the future due to more scrapped products coming from steel produced from scrap, and increased demands on the steel products produced.

PI has historically been traded at 40-100 USD over a premium scrap (A3). Compared to the calculated premium of 50 USD it seems that the market appreciates the known analysis of PI compared to scrap.

HDRI is mainly used in integrated DR-plants and the price is dependent on the price of natural gas. They seldom use large amounts of scrap, but that may be changed in the future. The value of the saved energy is obvious.

For CDRI it is worth noticing the value of an MgO content in the metal in order to decrease the amount of dolomite is here around 2 USD/ton. The benefits of having an MgO saturated primary slag at meltdown is well known but does not generate a cost benefit in these calculations.

HBI is often used in smaller amounts to assess a low tramp element charge in many plants and traded at price levels far higher than the 230 USD estimated here. In

this case the silicon content and the resulting slag amount decreases the ViU drastically.

One might wonder if the data cannot be interpreted that there is a strong potential for a better scrap processing and sorting. Furthermore, that indicates better ways to measure the levels of tramp elements in old scrap. In a market survey by the International Iron Metallics Association, IIMA, PI is traded at a price 10% over the price of premium scrap whereas HBI is traded 10%-20% under the premium scrap [14] taking all aspects into account. The raw material users and traders might find it valuable to look at the ViU for the materials in order to establish a market price reflecting the value the different materials bring to the steelmakers.

In the end, it is not about whether to use scrap, PI or DRI, it is about the right price for different types of scrap, PI and DRI and to find an optimal mix.

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This presentation is based on:

Gyllenram R., Wei W, Jönsson P. Raw material assessment for electric arc furnace steelmaking, ICS, International Congress on Science and Technology of Steelmaking, Beijing May 12-14 2015.

Comments are welcome.